

Mass Transport Processes in Porous Media Part I - General Theory

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Hoersaalzentrum 403H, 11:30 – 12:40

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Outline

- Advection – Diff. / Disp. – Equation (ADE)
- Dispersion and Diffusion
- Sorption Isotherms and Decay

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Advection – Dispersion/Diffusion – Equation (ADE)

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Governing Equations

If you can only remember one equation, then the Reynolds Transport Theorem.

$$\frac{\partial}{\partial t} \int_{\Omega} \psi d\Omega = - \oint_{\partial\Omega} \Phi^{\psi} \cdot d\mathbf{S} + \int_{\Omega} q^{\psi} d\Omega \quad (\text{Eq. 0})$$

Or, you can remember a story.

$$\left\{ \begin{array}{l} \text{Rate of accumulation} \\ \text{for unknown } \Psi \\ \text{within the} \\ \text{volume } \Omega \end{array} \right\} = \left\{ \begin{array}{l} \text{Net influx of } \Psi \text{ into} \\ \text{the volume } \Omega \\ \text{through its} \\ \text{surface } S \end{array} \right\} + \left\{ \begin{array}{l} \text{Net rate of } \Psi \\ \text{production} \\ \text{within the} \\ \text{volume } \Omega \end{array} \right\}$$



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Governing Equations

Because of the Gauss Divergence Theorem.

$$\oint_{\partial\Omega} \Phi^{\psi} \cdot d\mathbf{S} = \int_{\Omega} \nabla \cdot \Phi^{\psi} d\Omega$$

So, our Eq. 0 becomes.

$$\frac{\partial}{\partial t} \int_{\Omega} \psi d\Omega = - \int_{\Omega} \nabla \cdot \Phi^{\psi} d\Omega + \int_{\Omega} q^{\psi} d\Omega \quad (\text{Eq. 1})$$

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Advection Diff./Disp. Equation

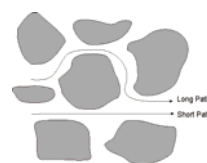
If we write Eq. 1 in derivative form,

$$\frac{\partial \psi}{\partial t} = \nabla \cdot (\Phi) + Q$$

Our primary unknown is Mass $\psi = n_e C dA$

Our flux is composed of:
1) Advective flux
2) Diff./ Disp. flux

Source / Sink



Advection (Mass takes a free ride)

$$\text{Flux of advection } F_{adv} = v_i n_e C dA$$

$$\text{Average Linear Velocity } v_x = \frac{K}{n_e} \frac{dh}{dl}$$

$$\text{AKA, Pore Velocity } v_x = \frac{q}{n_e} \leftarrow \text{Flux}$$

Velocity of a conservative tracer.

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OpenGeoSys Advection Diff./Disp. Equation

Exercise 0.1:

If only considers advection, how far does the Cl- go? Please draw it.

Conc. over Space

Conc. over Time

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Dispersion and Diffusion

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OpenGeoSys Dispersion and Diffusion

Diff./ Disp. Flux (Fick's 1st Law)

$$F_{diff} = -D \frac{dC}{dx} \quad 1D$$

$$F_{diff} = -D \nabla(C) \quad 3D$$

Think about: Why negative sign?

Hydrodynamic Dispersion (Mechanical spreading)

$$D_L = \alpha_L v_i + D^*$$

$$D_T = \alpha_T v_i + D^*$$

Diffusion coefficient
Longitudinal / transverse dispersivity

Note: Dispersivity values are often scale dependent!

$$\alpha_L = 0.83(\log L)^{2.414} \quad \text{Xu and Eckstein (1995)}$$

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OpenGeoSys Dispersion and Diffusion

Diffusion

Diffusion (Molecular spreading)

- It is orders magnitudes lower than dispersion effect.
- Need to be considered in no-flow conditions.
- Note: Temperature dependent.
- Use it with caution (e.g. charges in mineral structure)

Solute transport is from the left to the right: movement of the solutes is due to the concentration gradient (dC/dx).

Diffusion

Diffusion of ions in sea water and in deep-sea sediments

Table 1. Tracer and self-diffusion coefficients of ions at infinite dilution

Cation	D^0 (10 ⁻⁶ m²/sec)			Anion	D^0 (10 ⁻⁶ m²/sec)		
	0°C	18°C	25°C		0°C	18°C	25°C
H ⁺	36.1	31.7	30.1	OH ⁻	20.6	44.9	22.7
Li ⁺	4.72	9.89	10.3	F ⁻	—	12.1	14.6
Na ⁺	6.27	11.9	13.3	Cl ⁻	19.1	17.1	20.3
K ⁺	9.68	16.7	19.6	Br ⁻	16.5	17.6	20.1
Rb ⁺	10.6	17.6	20.6	I ⁻	16.9	17.5	20.0
Cs ⁺	10.6	17.7	20.7	NO ₃ ⁻	9.05	8.79	10.6
NH ₄ ⁺	9.80	16.6	19.4	SO ₄ ²⁻	9.75	14.4	17.3
Ag ⁺	6.80	14.0	16.6	SP ⁻	—	6.85	—
Tl ⁺	10.6	17.6	20.1	HCO ₃ ⁻	—	13.3	—
Cu(OH) ²⁺	—	—	9.30	NO ₂ ⁻	8.60	8.90	10.7
Zn(OH) ²⁺	—	—	8.54	BO ₂ ⁻	4.14	9.43	9.46
Ba ²⁺	—	9.44	9.43	NO ₂ ⁻	13.3	13.1	—
Mg ²⁺	3.06	3.94	7.05	NO ₃ ⁻	9.75	16.1	19.0
Ca ²⁺	3.73	6.75	7.93	NO ₂ ⁻	—	13.6	—
Fe ²⁺	3.73	6.70	7.94	CO ₃ ²⁻	6.39	7.80	9.65
Sn ²⁺	4.04	7.13	8.48	Fe ₂ SO ₄ ²⁻	—	7.13	9.46
Bi ³⁺	4.02	7.43	8.89	HPO ₄ ²⁻	—	—	7.34

Li Yuan-Hui, Sandra Gregory (1974) Diffusion of ions in sea water and in deep-sea sediments. *Geochimica et Cosmochimica Acta*, Volume 38, Issue 5, 703-714.

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Governing Equation with only dispersion / diffusion,

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2}$$

Analytical solution (Crank 1956)

$$C(x, t) = C_0 \operatorname{erfc}\left(\frac{x}{2\sqrt{Dt}}\right)$$

$$\operatorname{erfc}(B) = 1 - \operatorname{erf}(B)$$

$$\operatorname{erf}(B) = \frac{2}{\sqrt{\pi}} \int_0^B e^{-t^2} dt$$

Use a checking table, Or in Excel and other soft., it is provided.

The Advection - Dispersion / Diffusion equation,

$$\frac{\partial C}{\partial t} + v_x \frac{\partial C}{\partial x} - D \frac{\partial^2 C}{\partial x^2} = Q$$

Analytical solution (Ogata 1970)

$$C(x, t) = \frac{C_0}{2} \left[\operatorname{erfc}\left(\frac{L - v_x t}{2\sqrt{Dt}}\right) + \exp\left(\frac{v_x L}{D}\right) \operatorname{erfc}\left(\frac{L + v_x t}{2\sqrt{Dt}}\right) \right]$$

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Exercise 0.2:

Conc. over space at t1=1d and t2=2d

A point source

A continuous source

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Sorption Isotherms and Decay

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Sorption and Decay

Henry $C^* = K_D C$

Freundlich $C^* = K_1 C^{K_2}$

Langmuir $C^* = \frac{K_1 C}{1 + K_2 C}$

1st-order decay $\frac{\partial C}{\partial t} = -\lambda C$

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Sorption and Decay

Quick Question 1: What could be the unit of Henry sorption coefficient?

- A) mL/L;
- B) mg/L;
- C) mL/kg;
- D) g/g (-);
- E) m³/kg;

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Sorption and Decay

From KD to retardation factor.

What is the unit of retardation factor?

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Sorption and Decay

Quick Question 2: How can you quickly get λ values by the half life?

Try I-131, half life = **8.0197 days**
and Cs-137, half life = **30.17 years**

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Sorption and Decay

Exercise 3:

Effective Porosity = 0.3

NaCl = 0.1 M

1.0 m

Cross Section Area: 0.001 m²

Q = 0.003 m³/day

(1) Soil grain density is 2000 kg/m³, K_d = 2.0 mL/g, how much is the retardation factor R?

(2) What if there is a 1st order decay on the transported contaminant with ($\lambda = 0.7$ 1/day)

1.0

C/C₀

0

x

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